

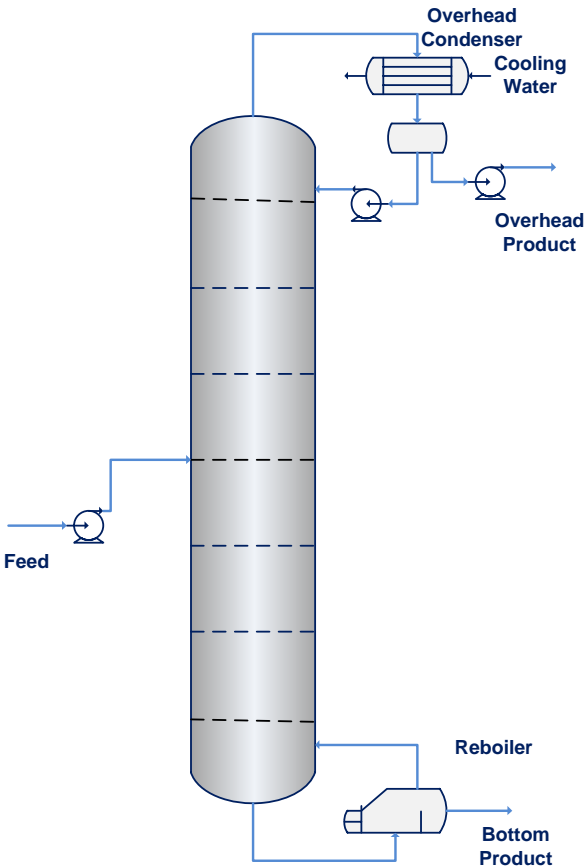
# Heat Integrated Distillation Columns (HIDC)

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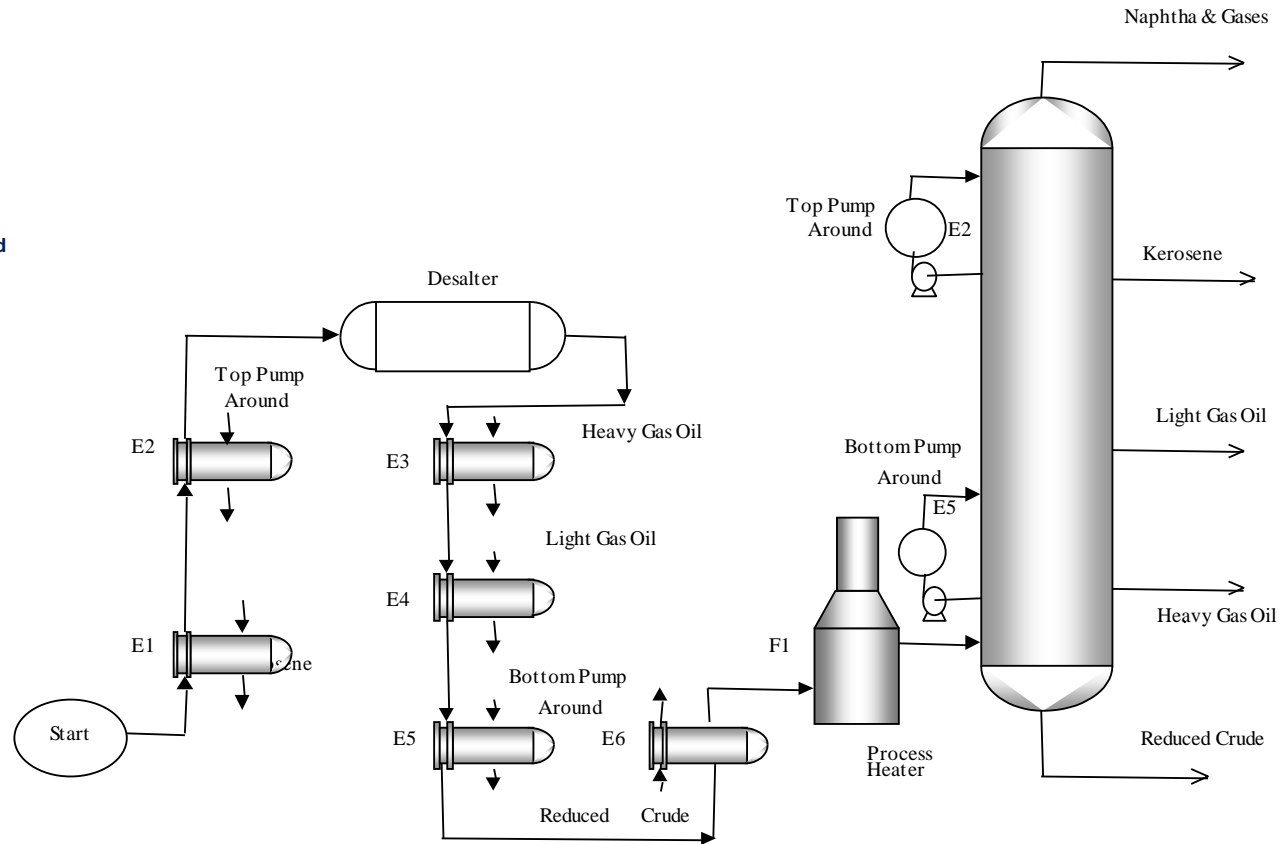
# Distillation in the Process Industry

- Separation processes to recover and purify account for over 40% of the Chemical Process Industry (CPI) energy demands
- Distillation is the dominate thermal separation process
- Process industry continues to enhance the energy efficiency of distillation by heat network, improved trays & packings and fouling mitigation, considered low-hanging fruits
- Application of reactive distillation is expected to expand for selective chemical synthesis processes
- Opportunities and challenging for new generation of distillation process for enhanced energy efficiency (i.e. reduced C-footprint) and synthesis of bio-based chemicals and capture & conversion of carbon dioxide to value-added products

# Conventional Distillation Process

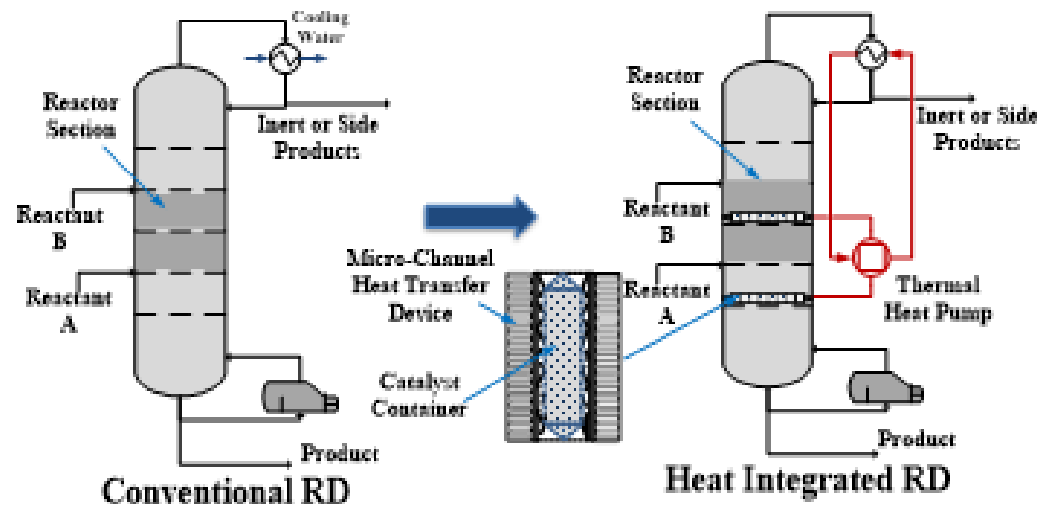
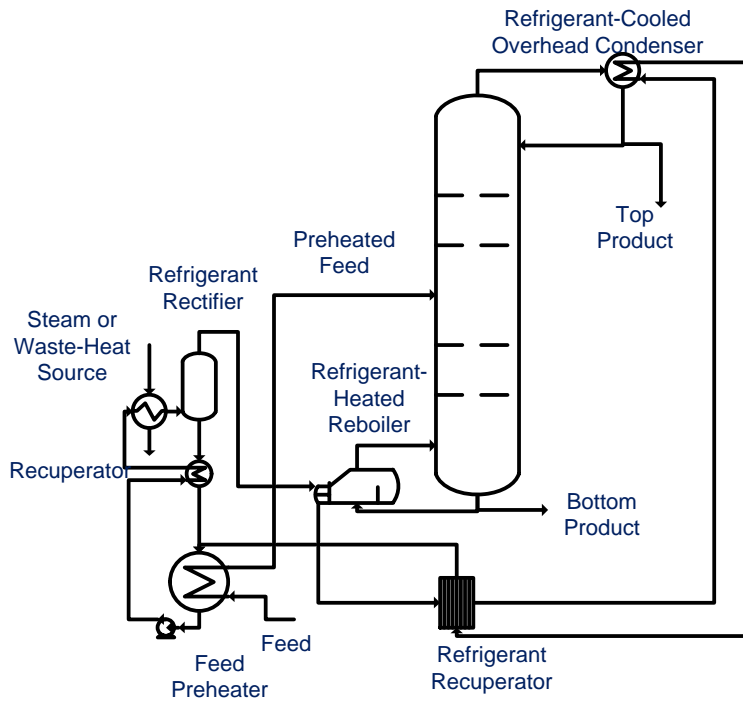


**Conventional Column**



**Crude Unit with HX Network**

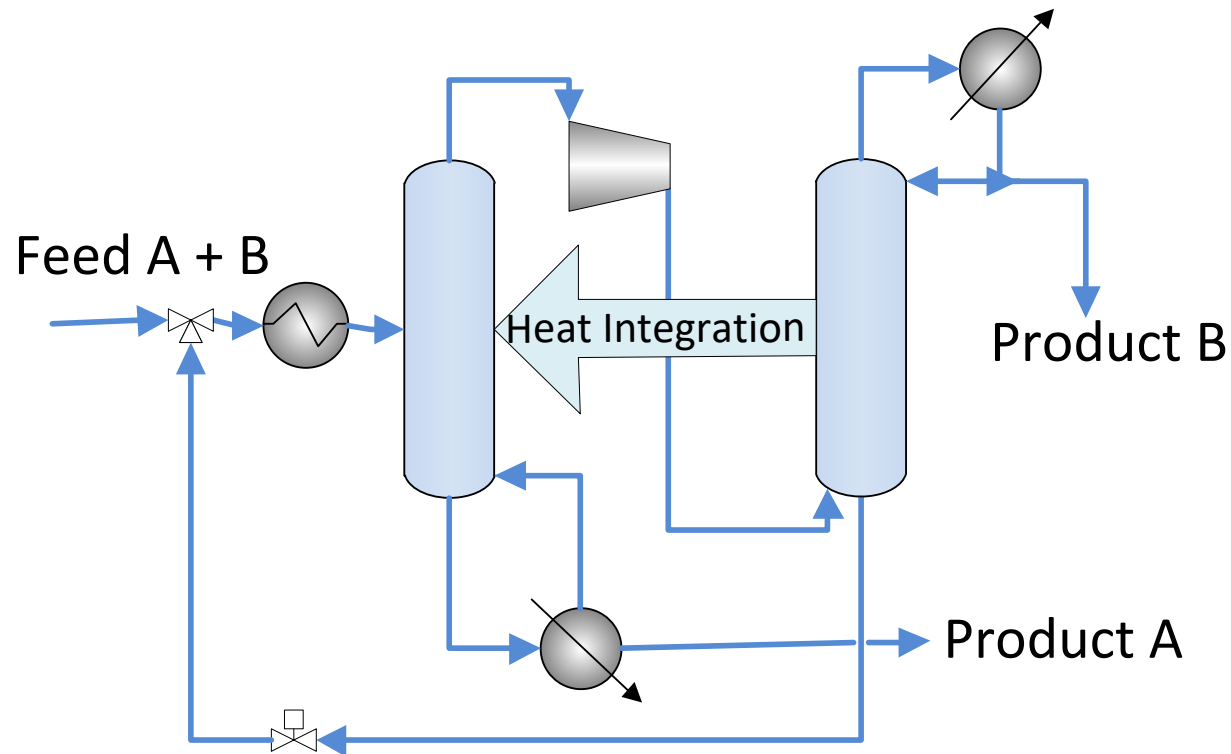
# Heat Integrated Distillation Columns (HIDC)



## Reactive Distillation Equipped with HIDC

### Recovery and Reuse of Latent Heat

# Thermally Coupled Column



*Transferring process heat from rectifier section to stripping section*

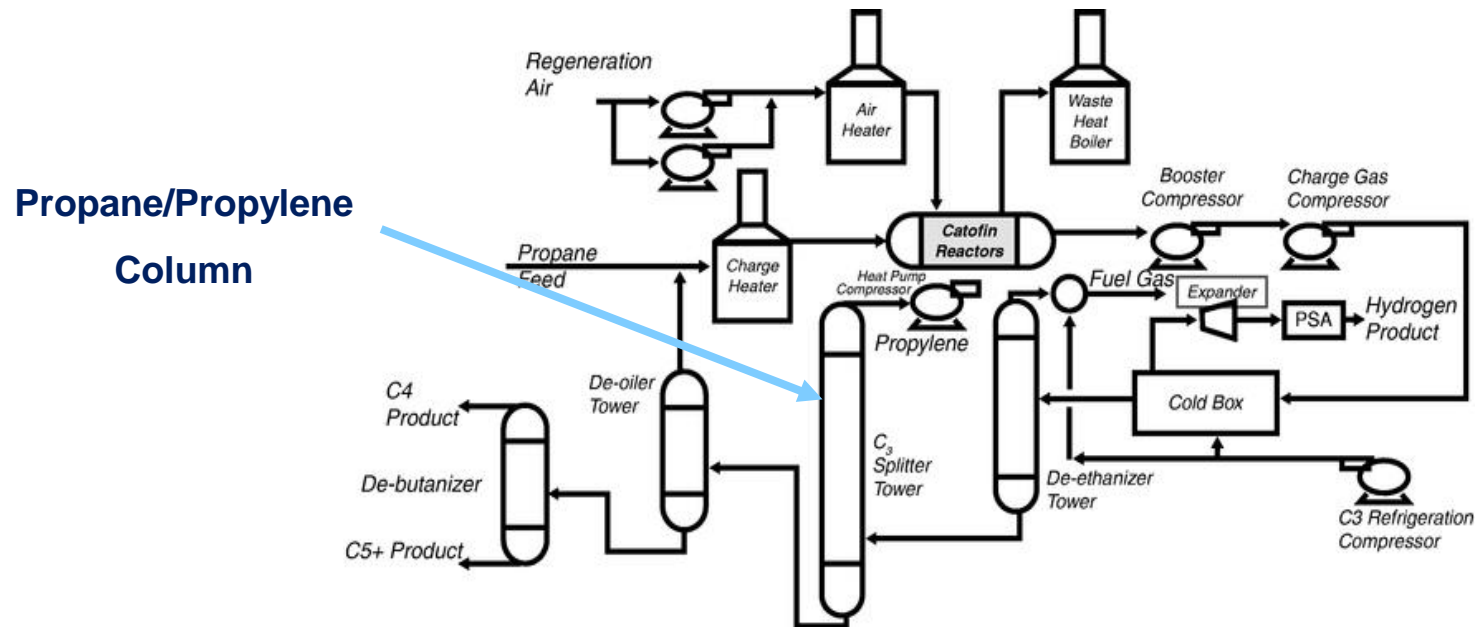
# Thermally Coupled Columns

## *Potential Applications*

- **Close boiling products such as propane/propylene hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>)/water (H<sub>2</sub>O)**
- **Separation of azeotropic mixtures such as dimethyl carbonate (DMC) and methanol**
- **Reactive distillation equipped with PerVaporization (PerVap) membrane separation**
- **Synthesis of bio-based specialty chemicals**

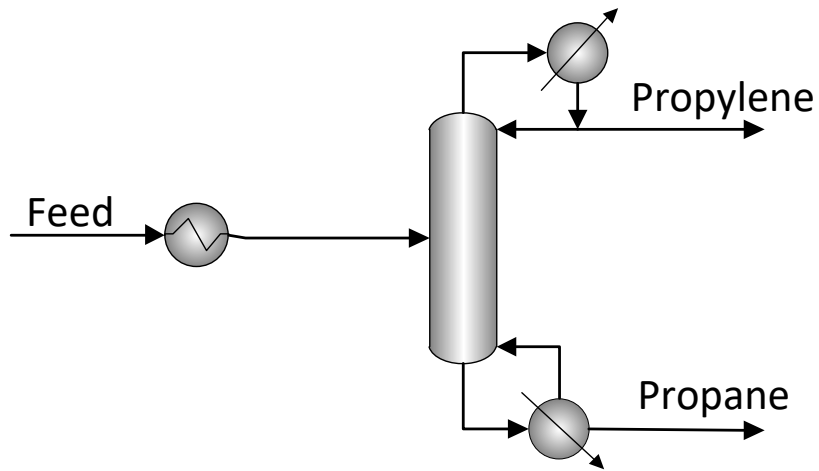
# Separation of Propane/Propylene

- Major petroleum chemical – propylene to polypropylene to consumer products
- Propylene is produced by de-hydrogenation of propane
- Boiling points – Propane  $-47.6\text{ C}$  Propylene  $-53.7\text{ C}$  at 1 atm.

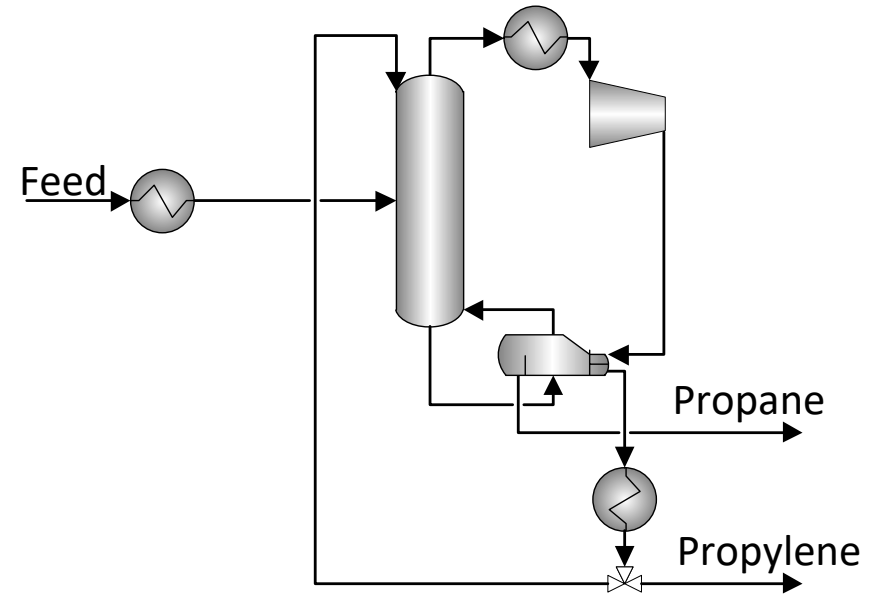


*Propylene is one of the large commodity chemicals*

# Separation of Propane/Propylene



**Conventional Distillation  
Process**

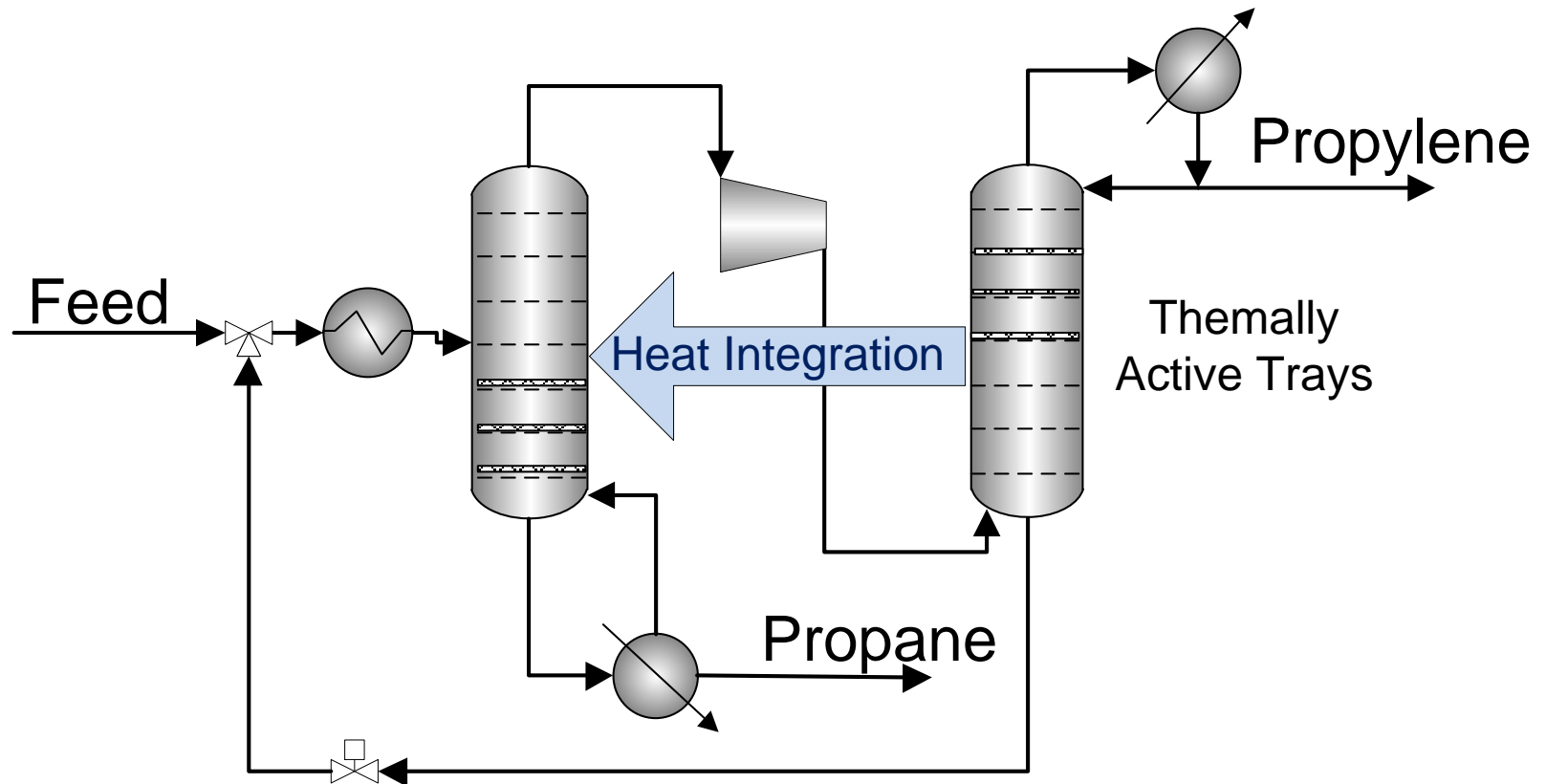


**Vapor Recompression  
(VCR) Heat Pump**

*VCR being Installed as retrofit with existing columns*



# Separation of Propane/Propylene



## Themally Coupled Distillation Columns

*Need to develop themally active trays & packings*

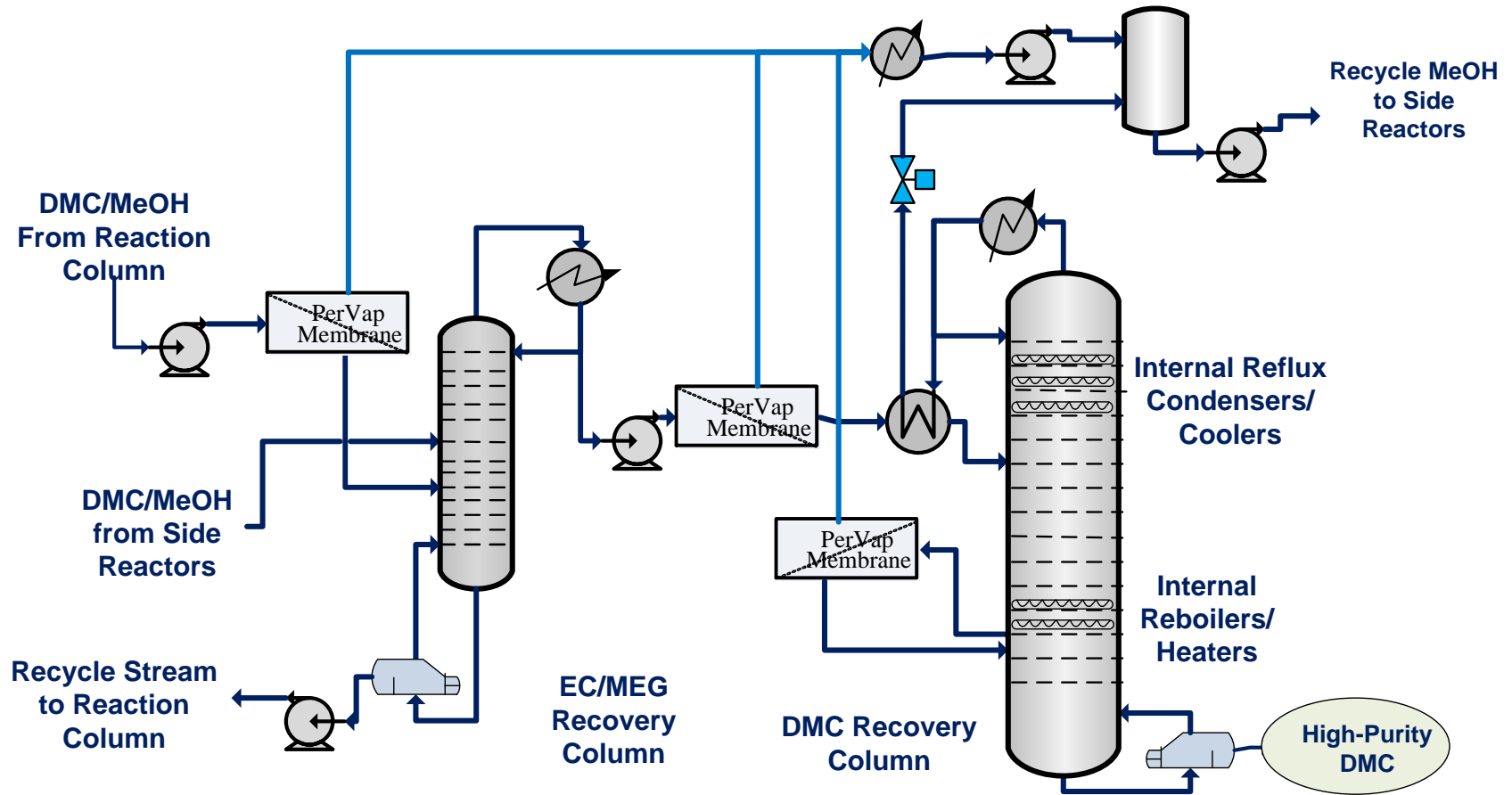
# Separation of Propane/Propylene

- **ASPEN Plus process simulation performed for the three separation processes**
- **Feed rate 21 tonnes/hr**
- **Composition – Propane 0.8 mass fraction**
- **Pressure for conventional distillation 18 bars**

# Separation of Propane/Propylene

		Conventional	Heat Pump	HIDiC
Utilities	Units	18 bar	18/30 bar	15/18 bar
Steam	tonnes/hr	35	2	5
Relative	%	100%	6%	15%
Cooling Water	tonnes/hr	1726	293	203
Relative	%	100%	17%	12%
Electric	kW	0	2822	1068
<b>Product Purity</b>				
Propane	wt%	97.5%	94.3%	95.0%
Propylene	wt%	98.5%	99.3%	97.3%
<b>CO<sub>2</sub> Emission</b>				
kg /hr		5452	2170	1341
kg CO <sub>2</sub> /kg Feed		0.26	0.10	0.06

# Separation of Azeotropic Mixture of Dimethyl Carbonate and Methanol



# Separation of Azeotropic Mixture of Dimethyl Carbonate and Methanol

	Baseline	HI & PerVap
<b>DMC Column Feed</b>		
Feed Rate, kg/hr	22,355	22,355
DMC, %wt	35.0%	35.0%
<b>Feed PerVap</b>		
Retendent DMC %wt	NA	40.0%
Permeate MeOH %wt	NA	99.4%
<b>Overhead Stream</b>		
OH Rate, kg/hr	16,040	12,827
DMC, %wt	9.7%	7.3%
DMC Flow Rate, kg/hr	1,563	931
<b>Bottom Product</b>		
Product Rate, kg/hr	6,313	6,933
DMC, %wt	99.9%	99.8%

# Separation of Azeotropic Mixture of Dimethyl Carbonate and Methanol

	Baseline	HI & PerVap
<b>Reboiler</b>		
Heat Duty, kW	6,460	5,860
Temperature, C	223.1	223.1
Internal Reboilers, kW	NA	200
<b>Overhead Condenser</b>		
Heat Duty, kW	4,850	3,960
Temperature, C	167.3	167.1
Internal Reflux Condensers	NA	600
PerVap Heat Duty, kW*	NA	600
Temperature, C	NA	106

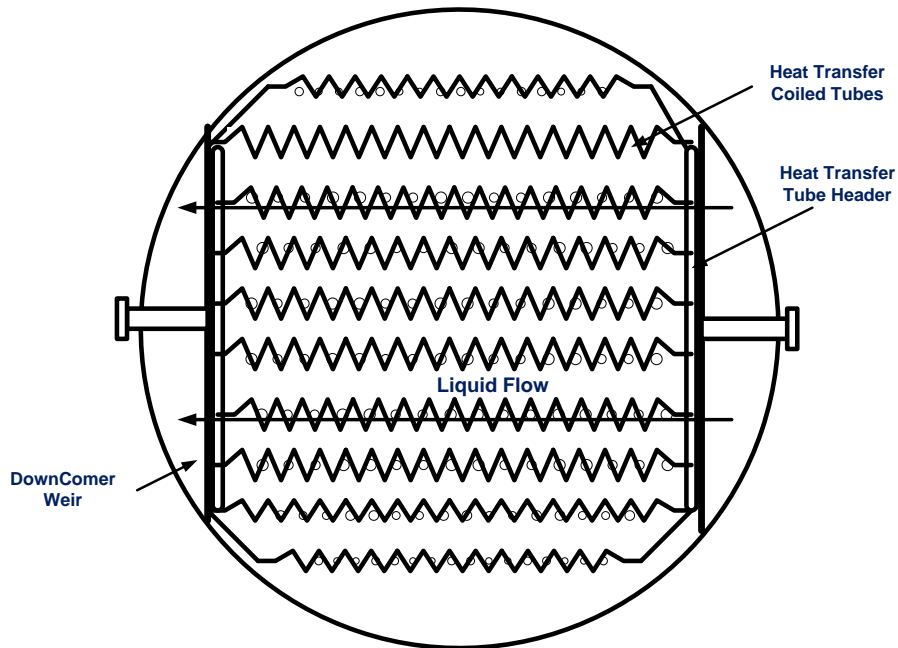
\* PerVap modules heat integrated with reflux condensers

# Thermally Active Trays and Packings

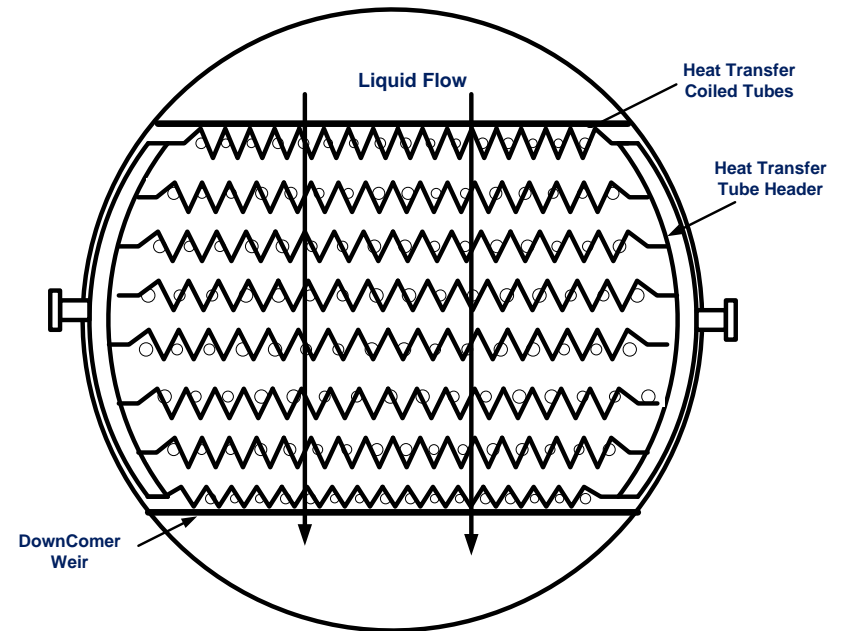
## Design Criteria and Technology Opportunities

- **Minimum impacts on vapor and liquid flows that may cause flooding**
- **High heat-transfer performance heat transfer to minimize size**
- **Configuration that can be integrated with trays and packings**
- **Effective integration with catalysts holding containers**
- **Heat transfer media can be liquid or phase-change media based on heat capacity requirements**
- **Potentially used of heat pipe with micro-channel flow passages**
- **Micro-channel device that can be manufactured by 3-D printing**

# Thermally Active Trays and Packings



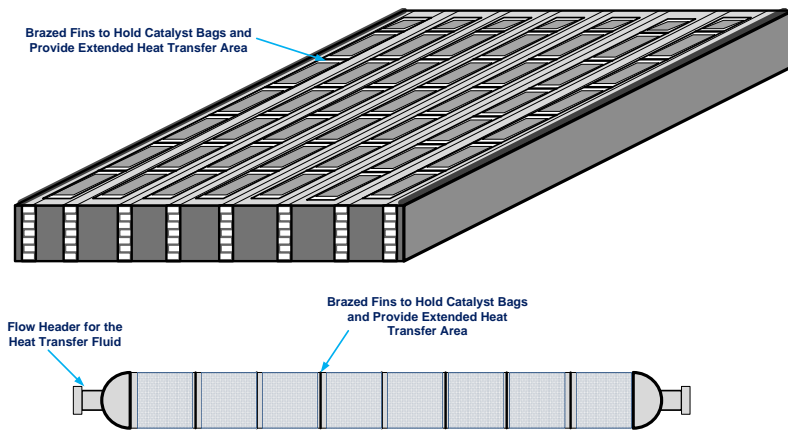
**Parallel Flow  
Configuration**



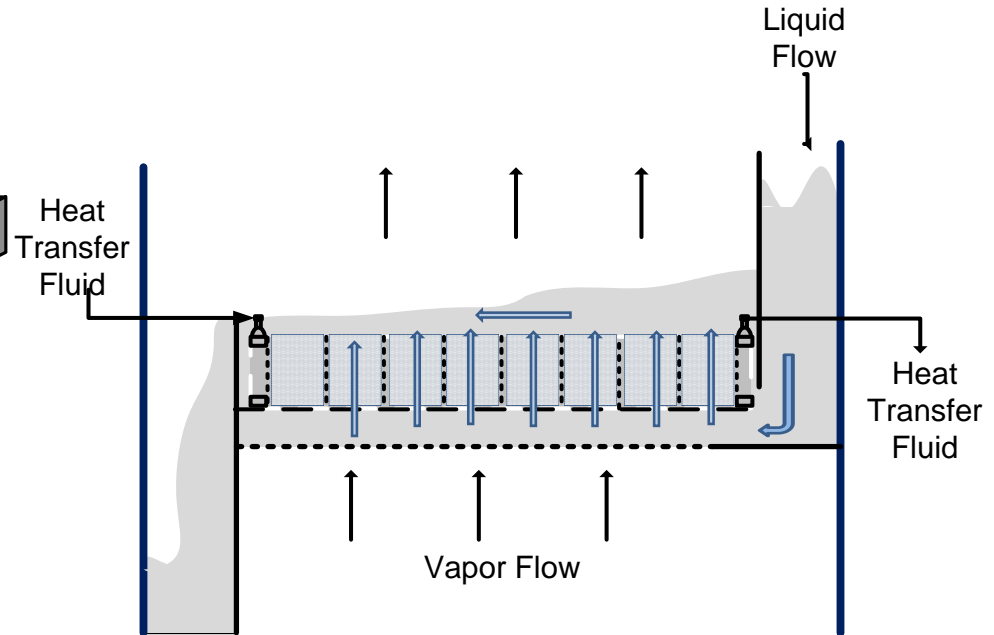
**Cross Flow  
Configuration**



# Thermally Active Trays and Packings



**Micro-Channel  
Brazed Unit**



**Compact HX  
Configuration**

# Conclusions and Path Forward

- **Thermally-coupled distillation columns enhances energy efficiency and potentially increased capacity**
- **Heat pipes can be integrated into divided-wall columns for an effective thermal management**
- **Development of heat-transfer devices for thermally-active distillation trays and packings**

